DIHYDROXystearic ACID (DHSA)
PRODUCTION BY IN SITU
HYDROLYSIS BASED ON OPTIMUM
PROCESS PARAMETERS OF
EPOXIDIZED PALM OIL-DERIVED
OLEIC ACID (EPOOA)

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Thesis submitted in fulfillment
of the requirements for the degree of
Doctor of Philosophy
(Chemical Engineering)

Faculty of Chemical Engineering

March 2021
AUTHOR’S DECLARATION

I declare that the work in this thesis was carried out in accordance with the regulations of Universiti Teknologi MARA. It is original and is the results of my own work, unless otherwise indicated or acknowledged as referenced work. This thesis has not been submitted to any other academic institution or non-academic institution for any degree or qualification.

I, hereby, acknowledge that I have been supplied with the Academic Rules and Regulations for Post Graduate, Universiti Teknologi MARA, regulating the conduct of my study and research.

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ABSTRACT

Owing to the increasing demands for eco-friendly epoxides derived from vegetable oils, much effort has been made regarding the epoxidation of palm oil in recent years. The oxirane rings are highly reactive to opening, especially through hydrolysis process to produced dihydroxystearic acid (DHSA). At present, there are no studies on the production of DHSA using \textit{in situ} hydrolysed epoxidized vegetable oil based on the optimum epoxidation process parameters. The aim of this study to produce \textit{in situ} hydrolysed DHSA from optimum process parameters of epoxidized palm oil-derived oleic acid (EPOOA). EPOOA was produced by using \textit{in situ} formed performic acid (PA). PA was formed by mixing formic acid (FA) as the oxygen carrier with hydrogen peroxide (HP) as the oxygen donor. The Taguchi method was used to optimize the epoxidation process for the maximum production of EPOOA. Then, \textit{in situ} hydrolysis was used to produce DHSA from optimized EPOOA. The signal to noise (S/N) ratio analysis in Taguchi method showed that the optimum process parameters for production of EPOOA to the response of relative conversion to oxirane (RCO) with determination of oxirane oxygen content (OOC) was maximum (85.6\%) under following conditions: (1) type of catalyst loading: sulphuric acid, (2) reaction temperature: 75°C, (3) stirring speed: 300 rpm, (4) FA/ oleic acid (OA) molar ratio: 1.0, and (5) HP/OA molar ratio: 1.5. The order of significance of the process parameters determined by analysis of variance (ANOVA) was as follows: catalyst type > stirring speed > HP/OA molar ratio > reaction temperature > FA/OA molar ratio. In addition, by using the optimized EPOOA, the effects of several process parameters (type of vegetable oil, oxidizing agents, catalyst concentration, HP concentration, type of process to produce the EPOOA, and hydrolysis method) on DHSA yield were studied. A mathematical model was developed by using the numerical integration Runge Kutta 4\textsuperscript{th} Order method. In this model, the method was integrated with genetic algorithm optimization to determine the process model that fit with the experimental data using MATLAB software. After 100 iterations, the reaction rate constant based on optimized EPOOA for DHSA production were obtained as follows: $k_{11} = 0.841 \text{ mol-L}^{-1}\cdot\text{min}^{-1}$, $k_{12} = 10.005 \text{ mol-L}^{-1}\cdot\text{min}^{-1}$, $k_{2} = 0.099 \text{ mol-L}^{-1}\cdot\text{min}^{-1}$, and $k_{3} = 0.011 \text{ mol-L}^{-1}\cdot\text{min}^{-1}$. Then, activation energy and thermodynamic analysis (enthalpy of activation, entropy of activation and free energy of activation) of DHSA production was identify based on Arrhenius equation. The results showed that there was good agreement between the simulation and experimental data, which validates the kinetic model. Overall, a high yield (80.7\% with purity 98.50\%) \textit{in situ} hydrolysed DHSA was successfully produced from POOA by using optimum process parameters of epoxidation.
ACKNOWLEDGEMENT

In the name of Allah, the Most Gracious, the Most Merciful. Allhamdulillah, all praises to Allah for His blessing, for the strength, and for the chances. He gave me over and over again in completing this thesis. My deepest gratitude goes to the two people that mean the world to me, my parents, Jalil Bin Miskin and Zaiton Binti Salim for their never-ending encouragement and support. Special thank also to my beloved wife, Intan Suhada Binti Azmi for caring me toward to complex my thesis.

My special appreciation goes to my supervisor, Assoc. Prof. Dr. Abdul Hadi for his guidance and patience. Thank you for not giving up on me. A sincere gratitude also goes to my co-supervisors, Assoc. Prof. Dr. Ir Chang Siu Hua, Aliff Farhan Mohd Yamin and Prof. Dr. Norhashimah Morad for suggestion and valuable advices.

My sincere thanks to the admiration team of Faculty of Chemical Engineering, UiTM Shah Alam and Cawangan Pulau Pinang. To those names left unmentioned but indirectly contributed to the birth of this thesis, thank you very much from the bottom of my heart.
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