

UNIVERSITI TEKNOLOGI MARA

**MODELLING AND CONTROL OF
DISTILLATION PLANT USING
FRACTIONAL-ORDER PID
CONTROLLER**

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the requirements for the degree of
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AUTHOR'S DECLARATION

I declare that the work in this dissertation was carried out in accordance with the regulations of Universiti Teknologi MARA. It is original and is the results of my own work, unless otherwise indicated or acknowledged as referenced work. This thesis has not been submitted to any other academic institution or non-academic institution for any degree or qualification.

I, hereby, acknowledge that I have been supplied with the Academic Rules and Regulations for Post Graduate, Universiti Teknologi MARA, regulating the conduct of my study and research.


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ABSTRACT

Over the recent years, there has been an explosive growth of interest in the usage of essential oil. Essential oils can be obtained through various type extraction techniques that ranging from conventional to modern techniques with the most common practice approach in extraction technology using steam distillation. Temperature is identified as the most influencing parameter in the quality of essential. Hence this study is focusing on the steam temperature control alone. The steam temperature exhibits nonlinear behaviour due to many factors. Previous studies have shown that fractional order control has the capability to handle the nonlinearity dynamic better than the conventional technique. Hence, the improvement of the control strategy is a necessary. This research presents the design of Fractional Order Proportional Integral Derivative (FOPID) with enhancement of low-pass filter and error filter for temperature regulation in a Small-Medium Industry Steam Distillation (SMISD) plant. There are several tests have been done to evaluate the performance of the developed controllers in the SMISD plant such as step test, set point change, and load disturbance test. The experiment was conducted in simulation and real-time environment. The results indicated that the system has a time constant of 796.86 s and dead time of 765.63 s. The Auto Regressive with eXogenous input (ARX) model that has been used to represent SMISD plant during the simulation study presented a good model fit with 99.24 %. The enhanced version of Model Predictive Controller (MPC) with anti-windup strategy has been introduced in this study which derived from Unconstrained MPC (UMPC) and Constrained MPC (CMPC). By integrating this strategy, it managed to stabilize the responses of UMPC controller towards step response and at the same time has a superior performance against the CMPC controller. The FOPID controller performance was successfully elevated by integrating error and low-pass filter. The error filter is responsible for eliminating persisting steady state error in fractional order controller while the low-pass filter is responsible for attenuating the effect of measurement of high frequencies noise. The improvement can be observed in simulation disturbance test where the FOPID with error and the low filter has better recover time of 12.32 % improvement compared with conventional FOPID. The performance FOPID and their variance also been benchmarked with conventional controllers (proportional controller) and advanced controllers (MPC controller) in simulation and real-time environment. The overall simulation experiments have shown the proposed FOPID-*ZNerlp* demonstrated the best performance under various test with a reduction in rise time, settling time, overshoot disturbance recovery time of 62.80 %, 87.50 %, 8.52 % and 70.30 % respectively. The real-time results have also shown agreement with reduction of 42.38 %, 65.20 %, 4.99 % and 62.92 % respectively.

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